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## Claims:

- 1. Method for producing ethanol and methane from biomass, comprising:
  - a) enzymatically liquefying and saccharifying flour of a biomass with a particle size of less than 1 mm in a conventional manner in the presence of water, thereby obtaining a mash;
  - b) fermenting and distilling the substrate in a conventional manner, thereby obtaining ethanol and a pulp;
  - c) separating the pulp into a solid phase and a clear phase, wherein a clear phase with a content of solids of less than 1% is obtained;
  - d) obtaining methane from the clear phase in a methane reactor.
- 2. Method according to claim 1, comprising milling biomass to a particle size of less than 1 mm, thereby producing flour.
- 3. Method according to any of the preceding claims, wherein hull components are substantially separated from the flour prior to step a, or separated from the mash prior to step b.
- 4. Method according to any of the preceding claims, wherein the biomass is grain.
- 5. Method according to any of the preceding claims, wherein grain, in particular wheat, rye, maize or triticales is used as biomass, and the bran is separated after milling.
- 6. Method according to any of the preceding claims, wherein the particle size of the flour is less than 0,6 mm.

- 7. Method according to any of the preceding claims, wherein proteins present in the biomass are substantially separated from the flour prior to step a or separated from the mash prior to step b or separated from the clear phase of the pulp in step c.
- 8. Method according to claim 7, wherein the separation of the proteins prior to step b comprises precipitation by cooling and separation of the precipitate.
- 9. Method according to claim 7, wherein the separation of the proteins in step c comprises precipitation by cooling and separation of the precipitate.
- 10. Method according to claim 9, wherein yeast, fibres, solid substances, fat and/or proteins present in the pulp are agglomerated by cooling and sedimented prior to separation of the pulp into solid phase and clear phase.
- 11. Method for producing ethanol und methane from grain, comprising
  - a) milling the grain to a particle size of less than 1 mm and separating the bran from the flour;
  - b) enzymatically liquefying and sacchariyfing the flour in a conventional manner in the presence of water, thereby obtaining a mash;
  - c) substantially precipitating the proteins present in the mash by cooling, sieving and drying, thereby obtaining the proteins and a substrate;
  - d) fermenting and distilling the substrate in a conventional manner, thereby obtaining ethanol and pulp;
  - e) separating the pulp into a solid phase and a clear phase, wherein a clear phase with a content of solids of less than 1% is obtained; and

- f) obtaining methane from the clear phase in a highperformance methane reactor.
- 12.Method according to any of the preceding claims, wherein a decanter or a disk centrifuge is used for separation of the solid phase and clear phase of the pulp.
- 13. Method according to any of the preceding claims, wherein about 80% of the liquid in the pulp is withdrawn with the clear phase.
- 14. Method according to any of the preceding claims, wherein the content of solids in the clear phase is less than 0,5%.
- 15. Method according to any of the preceding claims, wherein fermentation is carried out in a batch process, cascading process or in a continuous process comprising a recycling of yeast.
- 16.Method according to any of the preceding claims, wherein a high-performance methane reactor is employed.
- 17. Method for producing ethanol und methane from grain, comprising
  - a) milling the grain to a particle size of less than 1 mm, preferably less than 0,6 mm, and separating bran and hull components from the flour;
  - b) enzymatically liquefying and sacchariyfing the flour in a conventional manner in the presence of water, thereby obtaining a mash;
  - c) fermenting and distilling the substrate in a conventional manner, thereby obtaining ethanol and pulp;
  - d) agglomerating yeast, fibres, solid substances, fat and/or proteins present in the pulp by cooling and sedimenting them;

- e) dividing the pulp into a solid phase and a clear phase, wherein a clear phase with a content of solids of less than 1% is obtained; and
- f) obtaining methane from the clear phase in a highperformance methane reactor.
- 18. Method according to any of the preceding claims, wherein a high-performance methane reactor is employed, comprising beads with a diameter of 1 to 2 mm in which methane bacteria are immobilised.
- 19. Method according to claim 18, wherein the immobilisation of the methane bacteria in the beads increases the space time yield in the reactor and preferably allows a space time yield of at least 25 kg CSB/(m³\*d).
- 20. Method according to any of the preceding claims, wherein the methane production in a high-performance methane reactor comprises a pre-acidification / conditioning.
- 21. Method according to any of the preceding claims, wherein the high-performance methane reactor comprises an Upflow anaerobic sludge blanket (UASB)-reactor.
- 22. Method according to any of the preceding claims, wherein the high-performance methane reactor comprises an Internal Circulation (IC)-reactor.
- 23. Method according to any of the preceding claims, wherein the crude ethanol is rectified and, if necessary, dehydrated, in order to obtain bioethanol or neutral ethanol.
- 24. Method according to any of the preceding claims, wherein more than  $100 \text{ m}^3$  Ethanol / day are produced.
- 25. Method according to any of the preceding claims, wherein more than  $300~\text{m}^3$  Ethanol / day are produced.

- 26.Method according to any of the preceding claims, wherein the clear phase of the pulp is aerobically purified after anaerobic purification in the methane reactor.
- 27. Method according to claim 26, wherein the anaerobically/ aerobically purified clear phase is added to the conversion process as water for dilution.
- 28.Method according to any of claims 26 and 27, wherein anaerobically/aerobically purified clear phase is employed for the addition of water for liquefaction of the flour.
- 29. Method according to any of the preceding claims, wherein the solid phase of the pulp is mixed with separated hull components and/or bran.
- 30. Method according to any of the preceding claims, wherein the solid phase of the pulp is mixed with separated proteins.
- 31. Method according to claims 29 or 30, wherein the mixture is further dried.
- 32.Method for producing a feeding stuff and/or fertilizer comprising a method according to claims 29 to 31.
- 33. Method for producing energy and/or heat, comprising a method for producing ethanol and methane according to any of claims 1 to 32 and converting the methane to energy and/or heat.
- 34. Method according to claim 33, wherein the solid phase of the pulp is dried and burned for the generation of energy.
- 35. Method for producing energy and/or heat, comprising a method for producing ethanol and methane from grain, comprising
  - a) milling the grain to a particle size of less than 0,6 mm and separating bran and hull components from the flour;

- b) enzymatically liquefying and sacchariyfing the flour in a conventional manner in the presence of water, thereby obtaining a mash;
- c) fermenting and distilling the substrate in a conventional manner thereby obtaining ethanol and pulp;
- d) agglomerating yeast, fibers, solid substances, fat and/or proteins by cooling and sedimenting them;
- e) dividing the pulp into a solid phase and a clear phase, wherein a clear phase with a content of solids of less than 1% is obtained; and
- f) obtaining methane from the clear phase in a highperformance methane reactor and drying and burning the solid phase of the pulp for the generation of energy.
- 36.Use of the clear phase of pulp from the production of bioethanol with a content of solids of less than 1 % (w/v) for producing methane, energy and heat.
- 37. Use according to claim 36, wherein a high-performance methane reactor is employed for production of methane, comprising beads with a diameter of 1 to 2 mm in which methane bacteria are immobilised.
- 38.Use according to any of claims 36 and 37, wherein the immobilisation of the methane bacteria in the beads increases the space time yield in the reactor and preferably allows a space time yield of at least 25 kg  $CSB/(m^3*d)$ .
- 39. Use according to any of claims 36 to 38, wherein the method of preparing methane in a high-performance methane reactor comprises a pre-acidification / conditioning.

- 40. Use according to any of claims 36 to 39, wherein the high-performance methane reactor comprises an Upflow anaerobic sludge blanket (UASB) reactor.
- 41. Use according to any of claims 36 to 40, wherein the high-performance methane reactor comprises an Internal Circulation (IC) reactor.
- 42. Production plant for producing ethanol and methane from a biomass in accordance with any of claims 1 to 35 comprising a means for fermentation, distillation, and a high-performance methane reactor.
- 43. Ethanol, methane and/or energy obtainable according to any of claims 1 to 35.